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To: Assistant Commissioner for Patents  
Washington, D.C. 20231

Sir: Transmitted herewith for filing is the patent application of:

Inventor: SEE ATTACHED LIST (S. KANNO et al)

For:  
PROCESS FOR TREATING FLUORINE COMPOUND-CONTAINING GAS

Enclosed are:



9 Sheets of Drawings



This application is being filed without an executed Declaration.



Priority is claimed from Japanese Application No. 9-004349 & 9-163717  
filed 01/14/97 & 06/20/97. ☐ A certified copy is attached herewith.



Copies of the disclosure documents listed on the attached PTO 1449 form and  
☐ discussed in the specification or ☐ attached Information Disclosure Statement.



A verified statement to establish small entity status under 37 CFR 1.9 and 1.27.



Specification: Abstract ☒, Description ☒ 45 pages; and ☒ 21 claim(s).



Preliminary Amendment.



Executed Declaration.

The filing fee is calculated as shown below:

Small Entity

Large Entity

For:	No. Filed	No. Extra
Basic Fee		
Total Claims	21 - 20 =	* 1
Indep Claims	8 - 3 =	* 5
<input type="checkbox"/> Multiple Dependent Claim (s)		

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then enter '0' in second column

Rate	Fee
	\$ 395
x 11	\$
x 41	\$
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	\$ 790
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A check in the amount of \$ 1,222.00 is enclosed for the filing fee.



The Commissioner is hereby authorized to charge any additional fees that may be required to  
Deposit Account No. 02-1540. A duplicate of this sheet is attached.

Respectfully Submitted,

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## PROCESS FOR TREATING FLUORINE COMPOUND-CONTAINING GAS

## BACKGROUND OF THE INVENTION

## 1) Field of the Invention

The present invention relates to a process for efficient decomposition treatment of a gas containing  
5 fluorine compounds such as  $C_2F_6$ ,  $CF_4$ ,  $C_3F_8$ ,  $C_4F_8$ ,  $CHF_3$ ,  $SF_6$ ,  $NF_3$ , etc. at a low temperature.

## 2) Related Art

Fluorine compound gases such as  $CF_4$ ,  $C_2F_6$ , etc. are used in a large amount as a semiconductor etchant, a  
10 semiconductor cleaner, etc. However, it was found that these compounds, once discharged into the atmosphere, turn into warming substances causing global warming. Post-treatment of these compounds after their use would be subject to a strict control in the future.

15 Compounds having a high fluorine (F) content as a molecule constituent such as  $CF_4$ ,  $C_2F_6$ , etc. have a higher electronegativity of fluorine and thus are chemically very stable. From this nature it is very hard to decompose such fluorine compounds, and it is thus in  
20 the current situations that no appropriate processes for such decomposition treatment are not available yet.

JP-B-6-59388 (US Patent No. 5,176,897) discloses a  $TiO_2$ - $WO_3$  catalyst for hydrolysis of organic halogen compounds. The catalyst contains 0.1 to 20% by  
25 weight of W on the basis of  $TiO_2$  (i.e. 92% to 99.96% of Ti

by atom and 8 to 0.04% by atom of W) and has a decomposition rate of 99% at 375°C for a duration of 1,500 hours in treatment of  $\text{CCl}_4$  in ppm order. JP-B-6-59388 suggests that organic halogen compounds having a single carbon atom, such as  $\text{CF}_4$ ,  $\text{CCl}_2\text{F}_2$ , etc. can be decomposed, but shows no examples of decomposition results of fluorine compounds.

JP-A-7-80303 discloses another  $\text{Al}_2\text{O}_3\text{-ZrO}_2\text{-WO}_3$  catalyst for decomposition of fluorine compound gases.

10 The catalyst is directed to combustion-decomposition of CFCs (chlorofluorocarbons) and has a decomposition rate of 98% for a duration of 10 hours in treatment of CFC-115 ( $\text{C}_2\text{ClF}_5$ ) by combustion-decomposition reaction at 600°C. The disclosed process needs addition of hydrocarbons such

15 as n-butane, etc. as a combustion aid, resulting in a higher treatment cost. Among organic halogen compounds to be treated, fluorine compounds are less decomposable than chlorine compounds. Furthermore, the more the carbon atoms of organic halogen compound, the less

20 decomposable. Decomposition of compounds consisting only of carbon and fluorine such as  $\text{C}_2\text{F}_6$ , etc. are much less decomposable than CFC-115, but no examples of decomposition results of such compounds are shown therein.

## 25 SUMMARY OF THE INVENTION

An object of the present invention is to provide a process for efficient decomposition treatment

of compounds of carbon and fluorine, compounds of carbon, hydrogen and fluorine, compounds of sulfur and fluorine, compounds of nitrogen and fluorine and even compounds of carbon, hydrogen, fluorine and oxygen such as  $C_2F_6$ ,  $CF_4$ ,  
5  $C_3F_8$ ,  $C_4F_8$ ,  $CHF_3$ ,  $SF_6$  and  $NF_3$ .

The present invention provides a process for treating a fluorine compound-containing gas, which comprises contacting a gas stream containing at least one fluorine compound selected from the group consisting of  
10 compounds of carbon and fluorine, compounds of carbon, hydrogen and fluorine, compounds of sulfur and fluorine, compounds of nitrogen and fluorine and compounds of carbon, hydrogen, oxygen and fluorine with a catalyst containing at least one of alumina, titania, zirconia and  
15 silica in the presence of steam, thereby hydrolyzing the fluorine compound to convert fluorine of the fluorine compound to hydrogen fluoride.

#### BRIEF DESCRIPTION OF THE DRAWINGS

Fig. 1 is a block diagram showing a process for  
20 treating a fluorine compound-containing gas according to one embodiment of the present invention.

Fig. 2 is a graph showing performances of various catalysts for decomposing a fluorine compound.

Fig. 3 is a graph showing performances of  
25 various catalysts for decomposing a fluorine compound.

Fig. 4 is a graph showing performances of various catalysts for decomposing a fluorine compound.

Fig. 5 is a graph showing performances of various catalysts for decomposing a fluorine compound.

Fig. 6 is a graph showing performances of various catalysts for decomposing a fluorine gas.

5 Fig. 7 is a graph showing performance of catalysts with various composition ratios for decomposing a fluorine gas.

Fig. 8 is a graph showing performance of catalysts with various composition ratios for decomposing  
10 a fluorine gas.

Fig. 9 is a graph showing relations between reaction temperature and decomposition rate of various fluorine compounds.

Fig. 10 is a graph showing relations between  
15 reaction time and decomposition rate of a fluorine compound.

Fig. 11 is a graph showing relations between reaction temperature and decomposition rate of  $\text{CHF}_3$ ,  $\text{CF}_4$  and  $\text{C}_4\text{H}_8$  by an  $\text{Al}_2\text{O}_3$ -ZnO catalyst.

20 Fig. 12 is a graph showing relations between reaction temperature and decomposition rate of  $\text{SF}_6$  and  $\text{C}_3\text{F}_8$  by an  $\text{Al}_2\text{O}_3$ -NiO catalyst.

Fig. 13 is a graph showing relations between reaction temperature and decomposition rate of  $\text{C}_4\text{F}_8$  by an  
25  $\text{Al}_2\text{O}_3$ -NiO-ZnO catalyst.

#### DESCRIPTION OF THE PREFERRED EMBODIMENTS

As a result of extensive studies on development

of catalysts for decomposition of fluorine compound-  
containing gases, the present inventors have found that  
catalysts must contain a metallic component capable of  
forming an appropriately strong bond with fluorine as the  
5 nature of catalysts, and further have found that  
catalysts containing a metallic component having a higher  
fluoride formation enthalpy show a higher decomposition  
activity particularly in case of compounds consisting of  
carbon and fluorine, because molecules of such compounds  
10 are stable by themselves. Formation of too stable a bond  
will gradually lower the decomposition activity of  
catalysts, because fluorine compounds are less releasable  
from the catalyst surface, whereas too weak a bonding  
force will not attain a satisfactory decomposition rate.  
15  $C_2F_6$ , one of gases to be treated according to the present  
invention, is a compound of poor reactivity because of a  
higher intramolecular force, and it is said that a  
temperature of 1,500° to 2,000°C is required for combus-  
tion of such a gas.

20 As a result of tests on various catalysts, the  
present inventors have found that catalysts of alumina  
( $Al_2O_3$ ), titania ( $TiO_2$ ), zirconia ( $ZrO_2$ ), silica ( $SiO_2$ ), a  
mixture of titania and zirconia, a mixture of alumina and  
magnesia ( $MgO$ ), a mixture of alumina and titania, or a  
25 mixture of alumina and silica can hydrolyze fluorine  
compounds, and further have found that the fluorine  
compounds can be decomposed at a lower temperature than  
800°C thereby.



Among these catalysts, it has been found that a catalyst based on a mixture of alumina and titania has the highest activity and particularly a catalyst comprising 75 to 98% by weight of alumina and 25 to 2% by weight of titania has a particularly high activity. It can be presumed that the alumina of the catalyst based on a mixture of alumina and titania acts to attract fluorine compounds onto the catalyst, whereas the titania acts to depart the fluorine compounds from the catalyst surface.

10           The present inventors further have found that catalysts based on the mixture of alumina and titania further containing at least one member selected from the group consisting of zirconia, tungsten oxide, silica, tin oxide, ceria, bismuth oxide, nickel oxide and boron oxide  
15   can hydrolyze fluorine compounds. It has been found that above all the catalyst containing zirconia has a higher decomposition activity on fluorine compounds. It has been further found that the content of at least one member selected from the group consisting of zirconia,  
20   tungsten oxide, silica, tin oxide, ceria, bismuth oxide, nickel oxide and boron oxide is preferably 0.1 to 10% by weight on the basis of sum total of alumina and titania and particularly the content of zirconia is preferably 2 to 10% by weight on the basis of sum total of alumina and  
25   titania. It seems that these additive members exist in the form of single oxides or composite oxides and contribute to an improvement of decomposition activity on fluorine compounds.

In catalyst preparation, it has been found that it is preferable to use boehmite for alumina raw material and a titanium sulfate solution for a titania raw material. It has been confirmed that there are sulfate ions,  $\text{SO}_4^{2-}$ , in the catalysts prepared from the titanium sulfate solution and the decomposition activity on fluorine compounds can be improved by the presence of sulfate ions. It has been found that addition of sulfuric acid is preferable during the catalyst preparation.

The present inventors further tested catalysts containing other components besides alumina and titania, specifically catalysts containing alumina and one of zinc oxide ( $\text{ZnO}$ ), nickel oxide ( $\text{NiO}$ ), iron oxide, tin oxide ( $\text{SnO}_2$ ), platinum ( $\text{Pt}$ ), cobalt oxide, zirconia ( $\text{ZrO}_2$ ), ceria ( $\text{CeO}_2$ ) and silica ( $\text{SiO}_2$ ). As a result, it has been found that these catalysts can hydrolyze fluorine compounds and particularly catalysts containing zinc oxide or nickel oxide have a higher activity than catalysts based on the mixture of alumina and titania. It has been further found that catalysts comprising alumina and nickel oxide, admixed with sulfuric acid during the catalyst preparation have a higher activity than the catalyst without admixing with sulfuric acid. It has not been confirmed in which forms iron oxide or cobalt oxide of the catalysts containing the iron oxide or the cobalt oxide exists. Probably it seems to exist in the form of  $\text{Fe}_2\text{O}_3$  or  $\text{Co}_3\text{O}_4$ .

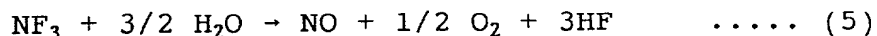
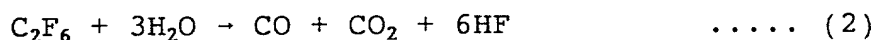
It has been found that the catalysts comprising alumina and one of Zinc oxide, nickel oxide, iron oxide, tin oxide, cobalt oxide, zirconia, ceria and silica as other components preferably contain 50 to 1% by atom of one metallic element of the other components, the balance being aluminum of the alumina, and the content of platinum is preferably 0.1 to 2% by weight on the basis (100% by weight) of alumina. It has been further found that these catalysts can further contain sulfur and the content of sulfur is preferably 0.1 to 20% by weight on the basis of the alumina catalyst.

Fluorine compounds to be treated according to the present invention include, for example,  $\text{CF}_4$ ,  $\text{C}_2\text{F}_6$ ,  $\text{C}_3\text{F}_8$ ,  $\text{C}_4\text{F}_{10}$ ,  $\text{C}_5\text{F}_{12}$ ,  $\text{CHF}_3$ ,  $\text{CH}_2\text{F}_2$ ,  $\text{CH}_3\text{F}$ ,  $\text{C}_2\text{HF}_5$ ,  $\text{C}_2\text{H}_2\text{F}_4$ ,  $\text{C}_2\text{H}_3\text{F}_3$ ,  $\text{C}_2\text{H}_4\text{F}_2$ ,  $\text{C}_2\text{H}_5\text{F}$ ,  $\text{CH}_2\text{OCF}_2$ ,  $\text{SF}_6$ ,  $\text{NF}_3$ , etc., among which  $\text{CF}_4$ ,  $\text{C}_2\text{F}_6$ ,  $\text{C}_3\text{F}_8$ ,  $\text{C}_4\text{F}_{10}$ ,  $\text{CHF}_3$ ,  $\text{SF}_6$  and  $\text{NF}_3$  are used as etchants for semiconductors and  $\text{CF}_4$ ,  $\text{C}_2\text{F}_6$  and  $\text{NF}_3$  are used as cleaners for semiconductors.

According to the present invention, all of these fluorine compounds can be hydrolyzed. Hydrolysis temperature depends upon kinds of fluorine compounds and catalyst components, and is usually  $200^\circ$  to  $800^\circ\text{C}$ , preferably  $400^\circ$  to  $800^\circ\text{C}$ . According to the present process fluorine of fluorine compound gases can be converted to hydrogen fluoride.

Hydrolysis of fluorine compounds can proceed typically according to the following reaction equations:





5           Hydrolysis according to reaction equations (2) and (3) can produce CO. The present catalysts also have an ability to oxidize CO, and thus CO can be further oxidized to CO<sub>2</sub> in the presence of oxygen.

          The present invention provides a process for  
10   hydrolyzing a fluorine compound-containing gas by a catalyst comprising at least one member selected from the group consisting of alumina, titania, zirconia, silica, a mixture of titania and zirconia, a mixture of alumina and magnesia, a mixture of alumina and titania and a mixture  
15   of alumina and silica.

          Furthermore, the present invention provides a process for treating a fluorine-containing gas by a catalyst comprising alumina and titania, further containing 0.1 to 10% by weight, on the basis of alumina and  
20   titania, of one of zirconia, tungsten oxide, silica, tin oxide, ceria, bismuth oxide, nickel oxide and boron oxide.

          Still furthermore, the present invention provides a process for treating a fluorine compound-  
25   containing gas by a catalyst comprising alumina and at least one member selected from the group consisting of zinc oxide, nickel oxide, iron oxide, tin oxide, cobalt oxide, zirconia, ceria, silica and platinum as other

components, a ratio of aluminum of alumina to the metallic element of at least one of other components by atom is 50 to 99 : 50 - 1, and further by the catalyst further containing 0.1 to 20% by weight of sulfur on the basis of the alumina. These additive components can contribute to improvement of decomposition activity of the catalysts on fluorine compounds in the form of single oxides or composite oxides with aluminum and/or other additive components.

Still furthermore, the present invention provides a process for converting fluorine in a gas to hydrogen fluoride, which comprises contacting a gas stream containing a fluorine compound comprising  $C_2F_6$  with a catalyst comprising a mixture of alumina and titania and having a weight ratio of alumina to titania being 65 to 90 : 35 to 10, thereby hydrolyzing the fluorine compounds. Still furthermore, the present invention provides a process for converting fluorine in a gas stream to hydrogen fluoride, which comprises contacting a gas stream comprising a fluorine compound comprising  $C_2F_6$  with a catalyst comprising a mixture of alumina, titania and zirconia and having a weight ratio of alumina to titania being 65 to 90 : 35 to 10 and a weight ratio of zirconia to sum total of alumina and titania being 2 to 10 : 98 to 90, thereby hydrolyzing the fluorine compound.

Still furthermore, the present invention provides a process for converting fluorine in a gas stream to hydrogen fluoride, which comprises contacting a

gas stream containing at least one fluorine compound  
selected from the group consisting of  $C_2F_6$ ,  $CF_4$ ,  $C_4F_8$  and  
 $CHF_3$  with a catalyst comprising a mixture of alumina and  
zinc oxide and having an atomic ratio of aluminum to zinc  
5 being 90 to 70 : 10 to 30, thereby hydrolyzing the  
fluorine compound.

Still furthermore, the present invention  
provides a process for converting fluorine in a gas  
stream to hydrogen fluoride, which comprises contacting a  
10 gas stream containing at least one fluorine compound  
selected from the group consisting of  $C_2F_6$ ,  $CF_4$ ,  $C_3F_8$ ,  $CHF_3$ ,  
 $NF_3$  and  $SF_6$  with a catalyst comprising a mixture of  
alumina and nickel oxide and having an atomic ratio of  
aluminum to nickel of 95 to 60 : 5 to 40, thereby  
15 hydrolyzing the fluorine compound.

Still furthermore, the present invention  
provides a process for converting fluorine in a gas  
stream to hydrogen fluoride, which comprises contacting a  
gas stream comprising a fluorine compound comprising  $C_4F_8$   
20 with a catalyst comprising a mixture of alumina, nickel  
oxide and zinc oxide, thereby hydrolyzing the fluorine  
compound.

Still furthermore, the present invention  
provides a process for converting fluorine in a gas  
25 stream to hydrogen fluoride, which comprises a hydrolysis  
step of contacting a gas discharged from a semiconductor-  
etching or cleaning step using a gas stream containing at  
least one fluorine compound selected from the group

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consisting of compounds of carbon and fluorine, compounds of carbon, hydrogen and fluorine, compounds of sulfur and fluorine, compounds of nitrogen and fluorine and compounds of carbon, hydrogen, oxygen and fluorine, after  
5 addition of air and steam to the gas, with a catalyst comprising at least one of alumina, titania, zirconia and silica, thereby hydrolyzing the fluorine compound to convert the fluorine in the gas to hydrogen fluoride, as a poststep to the semiconductor-etching or cleaning step.

10 Still furthermore, the present invention provide a process for treating a fluorine compound-containing gas, which further comprises an alkaline washing step of contacting the gas from the hydrolysis step with an alkaline washing solution, thereby washing  
15 the gas as a poststep to the hydrolysis step. As the alkaline washing solution, there can be used conventional ones such as a solution of NaOH,  $\text{Ca(OH)}_2$ ,  $\text{Mg(OH)}_2$ ,  $\text{CaCO}_3$ , etc., a slurry of  $\text{Ca(OH)}_2$ , etc.

In contacting of the gas stream containing a  
20 fluorine compound with the catalyst, the concentration of the fluorine compound in the gas stream is preferably 0.1 to 10% by volume, particularly preferably 0.1 to 3% by volume, and the space velocity is preferably 100 to 10,000  $\text{h}^{-1}$ , particularly preferably 100 to 3,000  $\text{h}^{-1}$ .  
25 Space velocity ( $\text{h}^{-1}$ ) is defined by reaction gas flow rate ( $\text{ml/h}$ )/catalyst volume ( $\text{ml}$ ).

In the hydrolysis of the fluorine compound, it is desirable to add steam as a hydrogen source for

hydrolysis to the gas stream so as to make the amount of hydrogen atoms (H) at least equal to the amount of fluorine atoms (F) contained in the fluorine compound, thereby making the fluorine atoms (F) of decomposition products into the hydrogen fluoride (HF) form that allows easy post-treatment. Hydrogen, hydrocarbons, etc. can be used as a hydrogen source besides the steam. In case of hydrocarbons as a hydrogen source, hydrocarbons can be combusted on the catalyst, thereby effectively reducing the heat energy to be supplied.

By adding an oxidizing gas such as oxygen, etc. to the reaction gas, oxidation reaction of CO can be carried out at the same time. When the oxidation reaction of CO is incomplete, the decomposition product gas is brought into contact with the CO oxidizing catalyst, after removal of HF from the decomposition product gas, to convert CO to CO<sub>2</sub>.

In the hydrolysis (decomposition) of fluorine compound, the reaction temperature is preferably about 200° to about 800°C. Above about 800°C, a higher decomposition rate can be obtained, but the catalyst will be rapidly deteriorated, and also the corrosion rate of apparatus structural materials will be abruptly increased, whereas below about 200°C the decomposition rate will be lowered.

As the step of neutralizing and removing the formed HF, washing by spraying an alkaline solution is efficient and preferable because of less occurrence of



clogging in pipings due to crystal deposition, etc.  
Bubbling of the decomposition product gas through the  
alkaline solution or washing with the alkaline solution  
through a packed column may be used for the neutraliza-  
5 tion and removal of the formed HF. Alternatively, HF can  
be absorbed in water, followed by treatment with an  
alkaline solution or slurry.

As the raw material for aluminum (Al) for  
preparing the present catalyst,  $\gamma$ -alumina and a mixture  
10 of  $\gamma$ -alumina and  $\delta$ -alumina can be used besides boehmite.  
However, it is preferable to use boehmite as a raw  
material for Al to form an oxide through final firing.

As the raw material for titanium (Ti), titania  
sol, titanium slurry, etc. can be used besides titanium  
15 sulfate.

As the third metallic components for silica  
(Si), magnesium (Mg), zirconium (Zr), etc., their various  
nitrates, ammonium salts, chlorides, etc. can be used.

The present catalyst can be prepared by any of  
20 ordinary procedures for preparing catalysts, such as  
precipitation, impregnation, kneading, etc.

The present catalyst can be used as such or  
upon molding into a granular form, a honeycomb form, etc.  
by an desired molding procedure such as extrusion  
25 molding, tableting, tumbling granulation, etc., or as a  
coating on ceramic or metallic honeycombs or plates.

Only a catalytic reactor for decomposing  
fluorine compounds and a facility for neutralizing and

removing acid components in the decomposition product gas are required for an apparatus for carrying out the present process for treating fluorine compound-containing gas.

5           The present invention will be described in detail below, referring to Examples which are not limitative of the present invention.

Fig. 1 shows an example of using the present process for hydrolysis treatment of a fluorine gas in a  
10 cleaning step in a plasma CVD apparatus in the semiconductor production process.

The plasma CVD apparatus is an apparatus for vapor depositing a  $\text{SiO}_2$  film on a semiconductor wafer surface. Since the  $\text{SiO}_2$  film tends to deposit on the  
15 entire interior surfaces of the apparatus, and thus it is necessary to remove  $\text{SiO}_2$  depositions from unwanted surfaces. To clean the unwanted surface to remove  $\text{SiO}_2$  therefrom, gases containing fluorine compounds such as  $\text{C}_2\text{F}_6$ ,  $\text{CF}_4$ ,  $\text{NF}_3$ , etc. are used as a cleaning gas. Cleaning  
20 gas 1 containing these fluorine compounds is led to a CVD chamber to remove  $\text{SiO}_2$  under plasma excitation. Then, the chamber is flushed with a  $\text{N}_2$  gas 2, thereby diluting the cleaning gas to a desired lower fluorine compound concentration, and the diluted cleaning gas is discharged  
25 from the chamber. The discharged gas is admixed with air 3 to further lower the fluorine compound concentration by dilution with air 3 and the air-diluted discharged gas is further admixed with steam 4 and the resulting reaction

gas 5 is led to a decomposition step, where the reaction gas is brought into contact with a catalyst at a desired space velocity ( $\text{h}^{-1}$ ), which is defined by reaction gas flow rate ( $\text{ml/h}$ )/catalyst volume ( $\text{ml}$ ) and at a desired temperature. In that case, the reaction gas may be heated or the catalyst may be heated by an electric oven, etc. The resulting decomposition gas 6 is led to an exhaust gas washing step, where the decomposition gas 6 is sprayed with an aqueous alkaline solution to remove acid components from the decomposition gas 6 and the resulting exhaust gas 7 freed from the acid components is discharged to the system outside.

$\text{CF}_4$ ,  $\text{C}_2\text{F}_6$  and  $\text{NF}_3$  can be used as etchants for semiconductors, etc., and  $\text{CHF}_3$ ,  $\text{C}_3\text{F}_8$ ,  $\text{SF}_6$  and  $\text{C}_4\text{F}_8$  can be also used as etchants besides the above-mentioned fluorine compounds. These etchants can be treated and decomposed in the same manner as in Fig. 1 except that the cleaning step of Fig. 1 is only replaced with an etching step.

Activities or performances of various catalysts for composing fluorine compounds were investigated, and results thereof will be described below:

#### Example 1

A  $\text{C}_2\text{F}_6$  gas having a purity of 99% or more was diluted with air, and further admixed with steam to prepare a reaction gas. Steam for the admixture was prepared by feeding pure water into a reactor tube from

the top at a flow rate of 0.11 ml/min. by a microtube pump and gasified. The reaction gas had a  $C_2F_6$  concentration of about 0.5%. Then, the reaction gas was brought into contact with various catalysts heated to 5 700°C in a reactor tube at a space velocity of 3,000 h<sup>-1</sup>. Heating of the catalyst was carried out by heating the reactor tube in an electric oven.

Reactor tube was an Inconel reactor tube having an inner diameter of 19 mm, where a catalyst bed was 10 fixed at the center of the reactor tube and had an Inconel thermowell for a thermo couple, 3 mm in outer diameter, inside the catalyst bed. Decomposition product gas discharged from the catalyst bed was bubbled through an aqueous sodium chloride solution and then discharged as 15 an exhaust gas.  $C_2F_6$  decomposition rate was calculated by the following equation by determining concentration of  $C_2F_6$  in the reaction gas at the inlet to the reactor tube and concentration of  $C_2F_6$  in the decomposition gas at the outlet from the alkaline washing step by FID (flame 20 ionization detector) gas chromatography and TCD (thermal conductivity detector) gas chromatography:

$$\text{Decomposition rate} = 1 - \frac{\text{Concentration of discharged fluorine compound}}{\text{Concentration of fed fluorine compound}} \times 100 (\%)$$

Catalyst 1 :  $Al_2O_3$

Granular alumina (NKHD-24, trademark of a 25 product commercially available from Sumitomo Chemical

Co., Ltd., Japan) was pulverized, sieved to obtain a fraction of 0.5 - 1 mm grain sizes, followed by drying at 120°C for 2 hours and firing (or calcining) at 700°C for 2 hours.

5 Catalyst 2 :  $\text{TiO}_2$

Granular titania (CS-200-24, trademark of a product commercially available from Sakai Chemical Industry Co., Ltd., Japan) was pulverized, sieved to obtain a fraction of 0.5 - 1 mm grain sizes, followed by  
10 drying at 120°C for 2 hours and firing at 700°C for 2 hours.

Catalyst 3 :  $\text{ZrO}_2$

200 g of zirconyl nitrate was dried at 120°C for 2 hours and fired at 700°C for 2 hours. The result-  
15 ing powders were placed in a mold and compression molded under a pressure of 500 kgf/cm<sup>2</sup>. The molded product was pulverized and sieved to obtain zirconia grains having grain sizes of 0.5 - 1 mm.

Catalyst 4 :  $\text{SiO}_2$

20 Granular silica (CARIAC-10, trademark of a product commercially available from Fuji Silysia Co., Ltd., Japan) was pulverized and sieved to obtain a fraction of 0.5 - 1 mm grain sizes, followed by drying at 120°C for 2 hours and firing at 700°C for 2 hours.

25 Catalyst 5 :  $\text{TiO}_2\text{-ZrO}_2$

Granular titania (CS-200-24) was pulverized to grain sizes of 0.5 mm and under. 100 g of the resulting powders was admixed with 78.3 g of zirconyl nitrate and

kneaded while adding pure water thereto. After the kneading, the kneaded mixture was dried at 120°C for 2 hours and fired at 700°C for 2 hours. The resulting powders were placed in a mold and compression molded  
5 under a pressure of 500 kgf/cm<sup>2</sup>. The molded product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm. The resulting grain composition for catalyst was in an atomic ratio of Ti : Zr = 81 : 19 and in a weight ratio of TiO<sub>2</sub> : ZrO<sub>2</sub> = 73.5 : 26.5.

10 Catalyst 6 : Al<sub>2</sub>O<sub>3</sub>-MgO

Granular alumina (NKHD-24) was pulverized to grain sizes of 0.5 mm and under. 100 g of the resulting powders were admixed with 56.4 g of magnesium nitrate and kneaded while adding pure water thereto. After the  
15 kneading, the kneaded mixture was dried at 120°C for 2 hours and fired at 700°C for 2 hours. The resulting powders were placed into a mold and compression molded under a pressure of 500 kgf/cm<sup>2</sup>. The molded product was pulverized and sieved to obtain grains having grain sizes  
20 of 0.5 - 1 mm. The resulting grain composition for catalyst was in an atomic ratio of Al : Mg = 90 : 10 and in a weight ratio of Al<sub>2</sub>O<sub>3</sub> : MgO = 91.9 : 8.1.

Catalyst 7 : Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub>

Granular alumina (NKHD-24) was pulverized to  
25 grain sizes of 0.5 mm and under. 100 g of the resulting powders were admixed with 17.4 g of dried powders of a metatitanic acid slurry and kneaded while adding pure water thereto. After the kneading, the kneaded mixture

was dried at 120°C for 2 hours and fired at 700°C for 2 hours. The resulting powders were placed in a mold and compression molded under a pressure of 500 kgf/cm<sup>2</sup>. The molded product was pulverized and sieved to obtain grains  
5 having grain sizes of 0.5 - 1 mm. The resulting grain composition for catalyst was in an atomic ratio of Al : Ti = 90 : 10 and in a weight ratio of Al<sub>2</sub>O<sub>3</sub> : TiO<sub>2</sub> = 85.2 : 14.8.

Catalyst 8 : Al<sub>2</sub>O<sub>3</sub>-SiO<sub>2</sub>

10 Granular alumina (NKHD-24) was pulverized to grain sizes of 0.5 mm and under. 100 g of the resulting powders were admixed with 13.2 g of dried powders of SiO<sub>2</sub> sol and kneaded while adding pure water thereto. After the kneading, the kneaded mixture was dried at 120°C for  
15 2 hours and fired at 700°C for 2 hours. The resulting powders were placed in a mold and compression molded under a pressure of 500 mgf/cm<sup>2</sup>. The molded product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm. The resulting grain composition for  
20 catalyst was in an atomic ratio of Al : Si = 90 : 10 and in a weight ratio of Al<sub>2</sub>O<sub>3</sub> : SiO<sub>2</sub> = 88.3 : 11.7.

Test results of the above-mentioned catalysts 1 to 8 are shown in Fig. 2, from which it is evident that the Al<sub>2</sub>O<sub>3</sub>-TiO catalyst is preferable as a hydrolysis  
25 catalyst for a C<sub>2</sub>F<sub>6</sub> gas.

#### Example 2

In this Example, influences of changes in

composition ratios of alumina to titania in  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  catalysts upon  $\text{C}_2\text{F}_6$  decomposition rate were investigated under the same test procedure and conditions as in Example 1. The results are shown in Fig. 4.

5 Catalyst 19 :  $\text{Al}_2\text{O}_3$

Boehmite powders (PURAL SB, trademark of a product commercially available from Condea Co., Ltd.) were dried at  $120^\circ\text{C}$  for 2 hours. 200 g of the resulting dried powders were fired at  $300^\circ\text{C}$  for 0.5 hours and  
10 further fired at an elevated temperature of  $700^\circ\text{C}$  for 2 hours. The resulting powders were placed into a mold and compression molded under a pressure of  $500 \text{ kgf/cm}^2$ . The molded product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm, and tested. It was  
15 found that boehmite powders used as an alumina raw material had a higher catalytic activity than granular alumina.

Catalyst 20 :  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$

Boehmite powders (PURAL SB) were dried at  $120^\circ\text{C}$   
20 for one hour. 200 g of the resulting dried powders were kneaded with 248.4 g of an aqueous 30% titanium sulfate solution, while adding about 200 g of pure water thereto. After the kneading, the kneaded mixture was dried at  $250^\circ$  -  $300^\circ\text{C}$  for about 5 hours and then fired at  $700^\circ\text{C}$  for 2  
25 hours. The resulting powders were placed into a mold and compression molded under a pressure of  $500 \text{ kgf/cm}^2$ . The molded product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm and tested. The result-



ing grain composition for catalyst was in an atomic ratio of  $Al : Ti = 90 : 10$  and in a weight ratio of  $Al_2O_3 : TiO_2 = 85.65 : 14.35$ .

Catalyst 21 :  $Al_2O_3-TiO_2$

5                   Boehmite powders (PURAL SB) were dried at  $120^\circ C$  for one hour. 200 g of the resulting dried powders were kneaded with about 100 g of an aqueous solution containing 78.6 g of 30% titania sol in pure water. After the kneading, the kneaded mixture was dried at  
10  $120^\circ C$  for about 2 hours and then fired at  $700^\circ C$  for 2 hours. The resulting powders were placed into a mold and compression molded under a pressure of  $500 \text{ kgf/cm}^2$ . The molded product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm and tested. The result-  
15 ing grain composition for catalyst was in an atomic ratio of  $Al : Ti = 91 : 9$  and in a weight ratio of  $Al_2O_3 : TiO_2 = 86.25 : 13.75$ .

It was found that the catalyst prepared from the titanium sulfate solution as a titanium raw material  
20 had the highest catalytic activity, probably because of the presence of sulfate ions  $SO_4^{2-}$  in the catalyst.

### Example 3

In this Example, influences of changes in composition ratios of  $Al_2O_3$  to  $TiO_2$  in  $Al_2O_3-TiO_2$  catalysts  
25 upon  $C_2F_6$  decomposition rate were investigated under the same procedure and conditions as in Example 1.

Catalyst 22 :  $\text{Al}_2\text{O}_3\text{-TiO}_2$

Boehmite powders (PURAL SB) were dried at  $120^\circ\text{C}$  for one hour. 100 g of the resulting dried powders were kneaded with 82.4 g of an aqueous 30% titanium sulfate solution while adding about 120 g of pure water thereto. After the kneading, the kneaded mixture was dried at  $250^\circ\text{C}$  -  $300^\circ\text{C}$  for about 5 hours and then fired at  $700^\circ\text{C}$  for 2 hours. The resulting powders were placed into a mold and compression molded under a pressure of  $500\text{ kgf/cm}^2$ . The molded product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm and tested. The resulting grain composition for catalyst was in an atomic ratio of  $\text{Al} : \text{Ti} = 93 : 7$  and in a weight ratio of  $\text{Al}_2\text{O}_3 : \text{TiO}_2 = 90.0 : 10.0$ .

Catalyst 23 :  $\text{Al}_2\text{O}_3\text{-TiO}_2$

Boehmite powders (PURAL SB) were dried at  $120^\circ\text{C}$  for one hour. 100 g of the resulting dried powders were kneaded with 174.4 g of an aqueous 30% titanium sulfate solution while adding about 70 g of pure water thereto. After the kneading, the kneaded mixture was dried at  $250^\circ\text{C}$  -  $300^\circ\text{C}$  for about 5 hours and then fired at  $700^\circ\text{C}$  for 2 hours. The resulting powders were placed into a mold and compression molded under a pressure of  $500\text{ kgf/cm}^2$ . The molded product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm and tested. The resulting grain composition for catalyst was in an atomic ratio of  $\text{Al} : \text{Ti} = 87 : 13$  and in a weight ratio of  $\text{Al}_2\text{O}_3 : \text{TiO}_2 = 80.9 : 19.1$ .

Catalyst 24 :  $\text{Al}_2\text{O}_3\text{-TiO}_2$

Boehmite powders (PURAL SB) were dried at  $120^\circ\text{C}$  for one hour. 100 g of the resulting dried powders were kneaded with 392 g of an aqueous 30% titanium sulfate solution while adding the latter to the former. After the kneading, the kneaded mixture was dried at  $250^\circ - 300^\circ\text{C}$  for about 5 hours and then fired at  $700^\circ\text{C}$  for 2 hours. The resulting powders were placed into a mold and compression molded under a pressure of  $500 \text{ kgf/cm}^2$ . The molded product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm and tested. The resulting grain composition for catalyst was in an atomic ratio of  $\text{Al} : \text{Ti} = 75 : 25$  and in a weight ratio of  $\text{Al}_2\text{O}_3 : \text{TiO}_2 = 65.4 : 34.6$ .

Activities of catalysts 19, 20 and 22-24 are shown in Fig. 5, from which is evident that the highest  $\text{C}_2\text{F}_6$  decomposition rate can be obtained at an alumina content of about 85% by weight.

#### Example 4

In this Example, an influence of sulfuric acid during the preparation of the  $\text{Al}_2\text{O}_3\text{-TiO}_2$  catalyst upon the  $\text{C}_2\text{F}_6$  decomposition rate was investigated.

Catalyst 25 :  $\text{Al}_2\text{O}_3\text{-TiO}_2$

Boehmite powders (PURAL SB) was dried at  $120^\circ\text{C}$  for one hour. 150 g of the resulting dried powders were kneaded with 58.5 g of 30% titania sol (CS-N, trademark of a product commercially available from Ishihara Sangyo

Kaisha, Ltd., Japan) and an aqueous solution prepared by diluting 44.8 g of 97% sulfuric acid with 250 ml of pure water. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 5 hours and then fired at 700°C  
5 for 2 hours. The resulting powders were placed into a mold and compression molded under a pressure of 500 kgf/cm<sup>2</sup>. The molded product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm and tested. The resulting grain composition for catalyst was  
10 in an atomic ratio of Al : Ti = 91 : 9 and in a weight ratio of Al<sub>2</sub>O<sub>3</sub> : TiO<sub>2</sub> = 86.3 : 13.7.

Sulfate ions were present in the catalyst. Test conditions were the same as in Example 1, except that the space velocity was changed to 1,000 h<sup>-1</sup>. The  
15 test results revealed that a C<sub>2</sub>F<sub>6</sub> decomposition rate of 80% was obtained at a reaction temperature of 650°C.

#### Example 5

In this Example, C<sub>2</sub>F<sub>6</sub> decomposition rates were investigated by adding various components to the  
20 Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> catalysts. The catalysts were prepared as follows, but test procedure and conditions were the same as in Example 1.

#### Catalyst 9 : Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub>

Granular alumina (NKHD-24) was pulverized and  
25 sieved to obtain grains having grain sizes of 0.5 - 1 mm, followed by drying at 120°C for 2 hours. Then, the dried grains were impregnated with 176 g of an aqueous 30%

titanium sulfate solution. After the impregnation, the grains were dried at 250° - 300°C for about 5 hours and then fired at 700°C for 2 hours. The resulting grain composition for catalyst was in an atomic ratio of Al : Ti = 90 : 10 and in a weight ratio of  $Al_2O_3$  :  $TiO_2$  = 85.1 : 14.9. The catalyst thus prepared was designated as catalyst A.

Catalyst 10 :  $Al_2O_3$ - $TiO_2$ - $ZrO_2$

50 g of Catalyst A grains were impregnated with an aqueous solution of 6.7 g of zirconyl nitrate dihydrate in 38.4 g of  $H_2O$ . After the impregnation, the grains were dried at 120°C for 2 hours and then fired at 700°C for 2 hours. The resulting grain composition for catalyst was in an atomic ratio of Al : Ti : Zr = 90 : 10 : 0.025 and in a weight ratio of  $Al_2O_3$  :  $TiO_2$  :  $ZrO_2$  = 80.2 : 14.0 : 5.8.

Catalyst 11 :  $Al_2O_3$ - $TiO_2$ - $WO_3$

50 g of Catalyst A grains were impregnated with 38.4 g of an aqueous solution of 6.5 g of ammonium paratungstate in  $H_2O$ . After the impregnation, the grains were dried at 120°C for 2 hours and then fired at 700°C for 2 hours. The resulting grain composition for catalyst was in an atomic ratio of Al : Ti : W = 90 : 10 : 0.025 and in a weight ratio of  $Al_2O_3$  :  $TiO_2$  :  $WO_3$  = 76.6 : 13.4 : 10.0.

Catalyst 12 :  $Al_2O_3$ - $TiO_2$ - $SiO_2$

50 g of Catalyst A grains were impregnated with 38.4 g of an aqueous solution of 7.5 g of 20 wt.% silica

sol in  $H_2O$ . After the impregnation, the grains were dried at  $120^\circ C$  for 2 hours and then fired at  $700^\circ C$  for 2 hours. The resulting grain composition for catalyst was in an atomic ratio of 90 : 10 : 0.025 and in a weight ratio of

5  $Al_2O_3 : TiO_2 : SiO_2 = 82.6 : 14.5 : 2.9$ .

Catalyst 13 :  $Al_2O_3-TiO_2-SnO_2$

50 g of Catalyst A grains were impregnated with 38.4 g of an aqueous solution of 5.6 g of tin chloride dihydrate in  $H_2O$ . After the impregnation, the grains were

10 dried at  $120^\circ C$  for 2 hours and then fired at  $700^\circ C$  for 2 hours. The resulting grain composition for catalyst was in an atomic ratio of Al : Ti : Sn = 90 : 10 : 0.025 and in a weight ratio of  $Al_2O_3 : TiO_2 : SnO_2 = 79.1 : 13.9 : 7.0$ .

15 Catalyst 14 :  $Al_2O_3-TiO_2-CeO_2$

50 g of Catalyst A grains were impregnated with 38.4 g of an aqueous solution of 10.9 g of cerium nitrate hexahydrate in  $H_2O$ . After the impregnation, the grains were dried at  $120^\circ C$  for 2 hours and then fired at  $700^\circ C$

20 for 2 hours. The resulting grain composition for catalyst was in an atomic ratio of Al : Ti : Ce = 90 : 10 : 0.025 and in a weight ratio of  $Al_2O_3 : TiO_2 : CeO_2 = 78.4 : 13.7 : 7.9$ .

Catalyst 15 :  $Al_2O_3-TiO_2-MnO_2$

25 50 g of Catalyst A grains were impregnated with 38.4 g of an aqueous solution of 7.2 g of manganese nitrate hexahydrate in  $H_2O$ . After the impregnation, the grains were dried at  $120^\circ C$  for 2 hours and then fired at

700°C for 2 hours. The resulting grain composition for catalyst was in an atomic ratio of Al : Ti : Mn = 90 : 10 : 0.025 and in a weight ratio of Al<sub>2</sub>O<sub>3</sub> : TiO<sub>2</sub> : MnO<sub>2</sub> = 81.6 : 14.3 : 4.1.

5 Catalyst 16 : Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub>-Bi<sub>2</sub>O<sub>3</sub>

50 g of Catalyst A grains were impregnated with 38.4 g of an aqueous solution of 12.13 g of bithmus nitrate hexahydrate in H<sub>2</sub>O. After the impregnation, the grains were dried at 120°C for 2 hours and then fired at 700°C for 2 hours. The resulting grain composition for catalyst was in an atomic ratio of Al : Ti : Bi = 90 : 10 : 0.025 and in a weight ratio of Al<sub>2</sub>O<sub>3</sub> : TiO<sub>2</sub> : Bi<sub>2</sub>O<sub>3</sub> = 85.1 : 14.8 : 1.1.

Catalyst 17 : Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub>-NiO

15 50 g of Catalyst A grains were impregnated with 38.4 g of an aqueous solution of 7.3 g of nickel nitrate hexahydrate in H<sub>2</sub>O. After the impregnation, the grains were dried at 120°C for 2 hours and then fired at 700°C for 2 hours. The resulting grain composition for catalyst was in an atomic ratio of Al : Ti : Ni = 90 : 10 : 0.025 and in a weight ratio of Al<sub>2</sub>O<sub>3</sub> : TiO<sub>2</sub> : NiO = 82.0 : 14.4 : 3.6.

Catalyst 18 : Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub>-BO<sub>4</sub>

25 50 g of Catalyst A grains were impregnated with 38.4 g of an aqueous solution of 1.36 g of ammonium borate octahydrate in H<sub>2</sub>O. After the impregnation, the grains were dried at 120°C for 2 hours and then fired at 700°C for 2 hours. The resulting grain composition for

catalyst was in an atomic ratio of Al : Ti : B = 90 : 10 : 0.005 and in a weight ratio of  $\text{Al}_2\text{O}_3$  :  $\text{TiO}_2$  :  $\text{BO}_3$  = 85.65 : 14.827 : 0.008.

It was found from Fig. 3 that the  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$ - $\text{ZrO}_2$  catalyst had the highest activity.

#### Example 6

In this Example, various catalysts containing alumina as one member were investigated for  $\text{C}_2\text{F}_6$  decomposition rates under the following conditions:

10 A  $\text{C}_2\text{F}_6$  gas having a purity of 99% or more was diluted with air, and the diluted gas was further admixed with steam to prepare a reaction gas. Steam was prepared by feeding pure water to a reactor tube from the top at a flow rate of about 0.2 ml/min. by a microtube pump to  
15 gasify the pure water. The reaction gas had a  $\text{C}_2\text{F}_6$  concentration of about 0.5%, and was brought into contact with a catalyst heated to 700°C by external heating of the reactor tube in an electric oven at a space velocity of 2,000  $\text{h}^{-1}$ .

20 The reactor tube was an Inconel reactor tube having an inner diameter of 32 mm and had a catalyst bed fixed at the center of the reactor tube. An Inconel thermowell for a thermocouple, 3 mm in diameter, was inserted into the catalyst bed. Decomposition product  
25 gas from the catalyst bed was bubbled through an aqueous calcium fluoride solution and discharged to the system outside.



The following catalysts were prepared for the test under the foregoing conditions:

Catalyst 26

Boehmite powders (PURAL SB) were dried at 120°C  
5 for one hour. 200 g of the resulting dried powders zinc  
nitrate hexahydrate and the mixture was kneaded. After  
the kneading, the kneaded mixture was dried at 250° -  
300°C for about 2 hours and then fired at 700°C for 2  
hours. The fired product was pulverized and sieved to  
10 obtain grains having grain sizes of 0.5 - 1 mm and  
tested. The resulting grain composition for catalyst was  
in an atomic ratio of Al : Zn = 91 : 9 and in a weight  
ratio of  $Al_2O_3$  : ZnO = 86.4 : 13.6.

Catalyst 27

15 Boehmite powders (PURAL SB) were dried at 120°C  
for one hour. 200 g of the resulting dried powders were  
admixed with an aqueous solution of 50.99 g of nickel  
sulfate hexahydrate and the mixture was kneaded. After  
the kneading, the kneaded mixture was dried at 250° -  
20 300°C for about 2 hours and then fired at 700°C for 2  
hours. The fired product was pulverized and sieved to  
obtain grains having grain sizes of 0.5 - 1 mm. The  
resulting grain composition for catalyst was in an atomic  
ratio of Al : Ni = 91 : 9 and in a weight ratio of  $Al_2O_3$  :  
25 NiO = 87.3 : 12.7.

Catalyst 28

Boehmite powder (PURAL SB) were dried at 120°C  
for one hour. 300 g of the resulting dried powders were

admixed with an aqueous solution of 125.04 g of nickel nitrate hexahydrate and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm. The resulting grain composition for catalyst was in an atomic ratio of Al : Ni = 91 : 9 and in a weight ratio of Al<sub>2</sub>O<sub>3</sub> : NiO = 87.3 : 12.7.

10 Catalyst 29

Boehmite powders (PURAL SB) were dried at 120°C for one hour. 300 g of the resulting dried powders were kneaded with 354.4 g of an aqueous 30% titanium sulfate solution while adding about 300 g of pure water thereto. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 5 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm and tested. The resulting grain composition for catalyst was in an atomic ratio of Al : Ti = 91 : 9 and in a weight ratio of Al<sub>2</sub>O<sub>3</sub> : TiO<sub>2</sub> = 86.6 : 13.4.

Catalyst 30

Boehmite powders (PURAL SB) were dried at 120°C for one hour. 200 g of the resulting dried powders were admixed with an aqueous solution of 115.95 g of iron nitrate nonahydrate and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then fired at 700°C for 2

hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm, and tested. The resulting grain composition was in an atomic ratio of Al : Fe = 91 : 9.

5 Catalyst 31

Boehmite powder (PURAL SB) were dried at 120°C for one hour. 200 g of the resulting dried powders were admixed with an aqueous solution of 95.43 g of tin chloride hydrate and the mixture was kneaded. After the  
10 kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then dried at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm and tested. The resulting grain composition for catalyst was in an atomic  
15 ratio of Al : Sn = 91 : 9 and in a weight ratio of Al<sub>2</sub>O<sub>3</sub> : SnO<sub>2</sub> = 77.4 : 22.6.

Catalyst 32

Boehmite powders (PURAL SB) were dried at 120°C for one hour. 200 g of the resulting dried powders were  
20 admixed with an aqueous solution prepared by diluting 22.2 g of a dinitrodiamino Pt(II) nitric acid solution (Pt concentration: 4.5 wt.%) with 200 ml of pure water, and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2  
25 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm and tested. The resulting grain composition for catalyst was in a weight ratio of

$\text{Al}_2\text{O}_3$  : Pt = 100 : 0.68.

#### Catalyst 33

Boehmite powders (PURAL SB) were dried at 120°C for one hour. 300 g of the resulting dried powders were  
5 admixed with an aqueous solution of 125.87 g of cobalt nitrate hexahydrate, and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to  
10 obtain grains having grain sizes of 0.5 - 1 mm and tested. The resulting grain composition was in an atomic ratio of Al : Co = 91 : 9.

#### Catalyst 34

Boehmite powder (PURAL SB) were dried at 120°C  
15 for one hour. 200 g of the resulting dried powders were admixed with an aqueous solution of 76.70 g of zirconyl nitrate dihydrate, and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then fired at 700°C for 2  
20 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm and tested. The resulting grain composition for catalyst was in an atomic ratio of Al : Zr = 91 : 9 and in a weight ratio of  $\text{Al}_2\text{O}_3$  :  $\text{ZrO}_2$  = 80.7 : 19.3.

#### 25 Catalyst 35

Boehmite powders (PURAL SB) were dried at 120°C for one hour. 200 g of the resulting dried powders were admixed with an aqueous solution of 124.62 g of cerium

nitrate hexahydrate, and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm and tested. The resulting grain composition for catalyst was in an atomic ratio of Al : Ce = 91 : 9 and in a weight ratio of  $\text{Al}_2\text{O}_3$  :  $\text{CeO}_2$  = 75.0 : 25.0.

#### Catalyst 36

Boehmite powders (PURAL SB) were dried at 120°C for one hour. 300 g of the resulting dried powders were admixed with an aqueous solution of 129.19 g of 20 wt.% silica sol, and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm and tested. The resulting grain composition for catalyst was in an atomic ratio of Al : Si = 91 : 9 and in a weight ratio of  $\text{Al}_2\text{O}_3$  :  $\text{SiO}_2$  = 89.6 : 10.4.

Test results of the foregoing catalysts 19 and 26 - 36 at a reaction temperature of 700°C are shown in Fig. 6,  $\text{C}_2\text{F}_6$  decomposition activity is highest with the  $\text{Al}_2\text{O}_3$ - $\text{ZnO}_2$  catalyst and is lowered in the order of the  $\text{Al}_2\text{O}_3$ -NiO catalyst, and the  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  catalyst. The highest activity of catalyst 26 seems to be due to the effect of S.

Example 7

In this Example, changes in the activity of  $\text{Al}_2\text{O}_3$ -NiO catalyst 28 were investigated by changing atomic ratios of Al : Ni. Test procedure and conditions were the same as in Example 6 except that the  $\text{C}_2\text{F}_6$  concentration was changed to 2% and the feed rate of pure water to 0.4 ml/min.

Catalyst 28-1

Boehmite powders (PURAL SB) were dried at 120°C for one hour. 200 g of the resulting dried powder were admixed with an aqueous solution of 8.52 g of nickel nitrate hexahydrate, and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm. The resulting grain composition for catalyst was in an atomic ratio of Al : Ni = 99 : 1 and in a weight ratio of  $\text{Al}_2\text{O}_3$  : NiO = 98.5 : 1.5.

Catalyst 28-2

Boehmite powders (PURAL SB) were dried at 120°C for one hour. 300 g of the resulting powders were admixed with an aqueous solution of 66.59 g of nickel nitrate hexahydrate, and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm. The

resulting grain composition for catalyst was in an atomic ratio of Al : Ni = 95 : 5 and in a weight ratio of  $Al_2O_3$  : NiO = 92.8 : 7.2.

#### Catalyst 28-3

- 5 Boehmite powders (PURAL SB) were dried at 120°C for one hour. 200 g of the resulting dried powders were admixed with an aqueous solution of 210.82 g of nickel nitrate hexahydrate, and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° -  
10 300°C for about 2 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm. The resulting grain composition for catalyst was in an atomic ratio of Al : Ni = 80 : 20 and in a weight ratio of  $Al_2O_3$   
15 : NiO = 73.2 : 26.8.

#### Catalyst 28-4

- Boehmite powders (PURAL SB) were dried at 120°C for one hour. 200 g of the resulting dried powders were admixed with an aqueous solution of 361.16 g of nickel  
20 nitrate hexahydrate, and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm. The  
25 resulting grain composition for catalyst was in an atomic ratio of Al : Ni = 70 : 30 and in a weight ratio of  $Al_2O_3$  : NiO = 61.4 : 38.6.

#### Catalyst 28-5

Boehmite powders (PURAL SB) were dried at 120°C for one hour. 200 g of the resulting dried powders were admixed with 562.1 g of nickel nitrate hexahydrate, and the mixture was kneaded while adding water thereto. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm. The resulting grain composition for catalyst was in an atomic ratio of Al : Ni = 60 : 40 and in a weight ratio of Al<sub>2</sub>O<sub>3</sub> : NiO = 50.6 : 49.4.

C<sub>2</sub>F<sub>6</sub> decomposition rate 6 hours after the start of test is shown in Fig. 7. It was found that the Ni content of Al<sub>2</sub>O<sub>3</sub>-NiO catalysts is in a range of 5 to 40 atom%, preferably 20 to 30 atom%.

#### Example 8

In this Example, changes in the activity of Al<sub>2</sub>O<sub>3</sub>-ZnO catalyst 26 was investigated by changing atomic ratios of Al : Zn. Test procedure and conditions were the same as in Example 6 except that the C<sub>2</sub>F<sub>6</sub> concentration was changed to 2% and the feed rate of pure water to 0.4 ml/min.

#### Catalyst 26-1

Boehmite powders (PURAL SB) were dried at 120°C for one hour. 200 g of the resulting dried powders were admixed with an aqueous solution of 215.68 g of zinc



nitrate hexahydrate and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to  
5 obtain grains having grain sizes of 0.5 - 1 mm. The resulting grain composition for catalyst was in an atomic ratio of Al : Zn = 80 : 20 and in a weight ratio of Al<sub>2</sub>O<sub>3</sub> : ZnO = 71.5 : 28.5.

#### Catalyst 26-2

10 Boehmite powders (PURAL SB) were dried at 120°C for one hour. 200 g of the resulting dried powders were admixed with 369.48 g of zinc nitrate hexahydrate and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and  
15 fired at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm. The resulting grain composition for catalyst was in an atomic ratio of Al : Zn = 70 : 30 and in a weight ratio of Al<sub>2</sub>O<sub>3</sub> : ZnO = 59.4 : 40.6.

#### 20 Catalyst 26-3

Boehmite powders (PURAL SB) were dried at 120°C for one hour. 126.65 g of the resulting dried powders were admixed with an aqueous solution of 96.39 g of zinc nitrate hexahydrate, and the mixture was kneaded. After  
25 the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm. The

resulting grain composition for catalyst was in an atomic ratio of Al : Zn = 85 : 15 and in a weight ratio of  $\text{Al}_2\text{O}_3$  : ZnO = 78.0 : 22.0.

$\text{C}_2\text{F}_6$  decomposition rate 6 hours after the start of test is shown in Fig. 8. It was found that the Zn content of  $\text{Al}_2\text{O}_3$ -ZnO catalysts is in a range of 10 to 30 atom%, preferably 10 to 15 atom%.

#### Example 9

In this Example, decomposition of  $\text{CF}_4$  and  $\text{CHF}_3$  was carried out with a  $\text{Al}_2\text{O}_3$ -NiO catalyst 28-3 under the same test procedure and conditions as in Example 6, except that the space velocity was changed to  $1,000 \text{ h}^{-1}$  and the fluorine compound was diluted with nitrogen in place of air. Test results at various reaction temperatures are shown in Fig. 9. It was found that the decomposition activity of  $\text{Al}_2\text{O}_3$ -NiO catalyst upon  $\text{CF}_4$  gas and  $\text{CHF}_3$  gas is higher than upon  $\text{C}_2\text{F}_6$  gas and the  $\text{Al}_2\text{O}_3$ -NiO catalyst is a preferable hydrolysis catalyst for  $\text{CF}_4$  or  $\text{CHF}_3$ . Furthermore, it was found that a preferable reaction temperature is  $600^\circ - 700^\circ\text{C}$  for the decomposition of  $\text{CF}_4$  and  $\text{CHF}_3$ , and  $650^\circ - 700^\circ\text{C}$  for the decomposition of  $\text{C}_2\text{F}_6$ . The higher the reaction temperature, the higher the decomposition rate. However, substantially 100% decomposition rate can be obtained at  $700^\circ\text{C}$ , and thus a higher reaction temperature than  $700^\circ\text{C}$  will be meaningless, and a reaction temperature must be as high

as 800°C.

#### Example 10

In this Example, influences of steam upon  $C_2F_6$  decomposition were investigated under the same test conditions as in Example 6 except that the space velocity was changed 1,000  $h^{-1}$ .  $Al_2O_3$ -NiO catalyst 28-3 was used at a reaction temperature of 700°C while supplying steam for 2 hours from the start of test, then interrupting supply of steam for 3 hours, and then starting to supply steam again. Test results are shown in Fig. 10. It was found that during the supply of steam the  $C_2F_6$  reaction rate was elevated due to the occurrence of  $C_2F_6$  hydrolysis.

#### Example 11

In this Example, decomposition of  $SF_6$  was investigated with  $Al_2O_3$ -NiO catalyst 28-3 under the same test conditions as in Example 6 except that a  $SF_6$  gas having a purity of 99% or more was used, the space velocity was changed to 1,000  $h^{-1}$  and the  $SF_6$  gas was diluted with nitrogen in of air. The reaction temperature was 700°C. Concentration of  $SF_6$  in the reaction gas at the inlet to the reactor tube and concentration of  $SF_6$  in the decomposition gas at the outlet from the alkaline washing step were determined by TCD gas chromatography and the decomposition rate was calculated by the following equation. It was found that the decomposition rate was 99% or more.

$$\text{Decomposition rate} = 1 - \frac{\text{Concentration of discharged SF}_6}{\text{Concentration of fed SF}_6} \times 100 (\%)$$

#### Example 12

In this Example, decomposition of NF<sub>3</sub> was investigated with Al<sub>2</sub>O<sub>3</sub>-NiO catalyst 28-3 under the same test conditions as in Example 11 except that a NF<sub>3</sub> gas having a purity of 99% or more was used. Reaction temperature was 700°C. Concentration of NF<sub>3</sub> in the reaction gas at the inlet to the reactor tube and concentration of NF<sub>3</sub> in the decomposition gas at the outlet from the alkaline washing step were determined by TCD gas chromatography and the decomposition rate was calculated according to the following equation. It was found that the decomposition rate was 99% or more. It was found preferable to carry out the decomposition of the NF<sub>3</sub> gas with the Al<sub>2</sub>O<sub>3</sub>-NiO catalyst at a temperature of 600° - 800°C.

$$\text{Decomposition rate} = \frac{\text{Concentration of discharged NF}_3}{\text{Concentration of fed NF}_3} \times 100 (\%)$$

#### Example 13

In this Example, activity of Al<sub>2</sub>O<sub>3</sub>-ZnO catalyst upon hydrolysis of a CF<sub>4</sub> gas, a C<sub>4</sub>F<sub>8</sub> gas and a CHF<sub>3</sub> gas was investigated. Decomposition of a CF<sub>4</sub> gas was carried out in the following manner:

At first, a  $\text{CF}_4$  gas having a purity of 99% or more was diluted with air, and the diluted  $\text{CF}_4$  gas was further admixed with steam. Concentration of  $\text{CF}_4$  in the reaction gas was about 0.5%, and steam flow rate was  
5 adjusted to about 50 times as high as that of the fluorine compound, i.e.  $\text{CF}_4$ . The reaction gas was brought into contact with the catalyst heated to a predetermined temperature in a reactor tube in an electric oven at a space velocity of  $1,000 \text{ h}^{-1}$ . Decomposition product gas  
10 from the catalyst bed was bubbled through an aqueous sodium hydroxide solution and then discharged to the system outside. Decomposition rate of  $\text{CF}_4$  was determined by TCD gas chromatography.

The  $\text{Al}_2\text{O}_3$ -ZnO catalyst used for the test was  
15 prepared in the following manner:

Boehmite powders (PURAL SB) were dried at  $120^\circ\text{C}$  for one hour. 126.65 g of the resulting dried powders were admixed with 96.39 g of zinc nitrate hexahydrate, and the mixture was kneaded. After the kneading, the  
20 kneaded mixture was dried at  $250^\circ - 300^\circ\text{C}$  for about 2 hours and then fired at  $700^\circ\text{C}$  for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm. The resulting grain composition for catalyst was in an atomic ratio of Al :  
25 Zn = 85 : 15 and in a weight ratio of  $\text{Al}_2\text{O}_3$  : ZnO = 78 : 22.

Fig. 11 shows decomposition rates of  $\text{CF}_4$  at various reaction temperatures and also those of  $\text{CHF}_3$  and

C<sub>4</sub>F<sub>8</sub> as fed and decomposed in the same manner as above. Decomposition rates of CHF<sub>3</sub> and C<sub>4</sub>F<sub>8</sub> were determined by FID gas chromatography, whereby it was found that the Al<sub>2</sub>O<sub>3</sub>-ZnO catalyst had a higher activity upon the CF<sub>4</sub> gas, 5 the C<sub>4</sub>F<sub>8</sub> gas and the CHF<sub>3</sub> gas. It was also found that a higher decomposition rate can be obtained preferably at a reaction temperature of 650°C or higher for the hydrolysis of the C<sub>4</sub>F<sub>8</sub> gas and even at a reactor temperature of 600°C or lower for the hydrolysis of the CHF<sub>3</sub> gas 10 or the CF<sub>4</sub> gas.

#### Example 14

In this Example, the decomposition activity of as Al<sub>2</sub>O<sub>3</sub>-NiO catalyst upon a C<sub>3</sub>F<sub>8</sub> gas, a C<sub>4</sub>F<sub>8</sub> gas and a SF<sub>6</sub> gas was investigated in the same manner as in Example 13. 15 The concentration of C<sub>4</sub>F<sub>8</sub> in the reaction gas after decomposition of C<sub>4</sub>F<sub>8</sub> was 0.1% by volume. The Al<sub>2</sub>O<sub>3</sub>-NiO catalyst used for the test was prepared in the following manner:

Boehmite powders (PURAL SB) were dried at 120°C 20 for one hour. 200 g of the resulting dried powders were admixed with an aqueous solution of 210.82 g of nickel nitrate hexahydrate, and the mixture was kneaded. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours, and then fired at 700°C for 2 25 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm. The resulting grain composition for catalyst was in an atomic

ratio of Al : Ni = 80 : 20 and in a weight ratio of  $\text{Al}_2\text{O}_3$  : NiO = 73.2 : 26.8.

Fig. 12 shows decomposition rates at various reaction temperatures, where the decomposition rate of  $\text{C}_3\text{F}_8$  and  $\text{C}_4\text{F}_8$  was determined by FID gas chromatography and that of  $\text{SF}_6$  by TCD gas chromatography. It was found from the test results that the  $\text{Al}_2\text{O}_3$ -NiO catalyst had a higher activity upon the hydrolysis of the  $\text{SF}_6$  gas,  $\text{C}_3\text{F}_8$  gas and the  $\text{C}_4\text{F}_8$  gas, and the reaction temperature was preferably 500°C or higher for the hydrolysis of the  $\text{SF}_6$  gas and preferably 700°C or higher for the hydrolysis of the  $\text{C}_3\text{F}_8$  gas. In the case of  $\text{C}_4\text{F}_8$  gas, the reaction temperature for the hydrolysis was preferably 650°C or higher.

#### Example 15

In this Example, decomposition activity of an  $\text{Al}_2\text{O}_3$ -NiO-ZnO catalyst upon  $\text{C}_4\text{F}_8$  was investigated in the same manner as in Example 13. The  $\text{Al}_2\text{O}_3$ -NiO-ZnO catalyst used for the test was prepared in the following manner:

Boehmite powders (PURAL SB) were dried at 120°C for one hour. 200 g of the resulting dried powders were admixed with 210.82 g of nickel nitrate hexahydrate and 152.31 g of zinc nitrate hexahydrate, and the mixture was kneaded while adding pure water thereto. After the kneading, the kneaded mixture was dried at 250° - 300°C for about 2 hours and then fired at 700°C for 2 hours. The fired product was pulverized and sieved to obtain grains having grain sizes of 0.5 - 1 mm. The resulting

grain composition for catalyst was in atomic ratios of Al : Ni = 80 : 20 and Al : Zn = 85 : 15 and in a weight ratio of  $\text{Al}_2\text{O}_3$  : NiO : ZnO = 60.7 : 22.2 : 17.1.

Fig. 13 shows decomposition rates at various  
5 reaction temperatures, where the decomposition rate of  $\text{C}_4\text{F}_8$  was determined by FID gas chromatography.



WHAT IS CLAIMED IS:

1. A process for treating a fluorine compound-containing gas, which comprises contacting a gas stream containing at least one of compounds of carbon and fluorine, compounds of carbon, hydrogen and fluorine, compounds of sulfur and fluorine, compounds of nitrogen and fluorine and compounds of carbon, hydrogen, oxygen and fluorine with a catalyst containing at least one of alumina, titania, zirconia and silica in the presence of steam, thereby hydrolyzing the fluorine compound to convert the fluorine of the fluorine compound to hydrogen fluoride.
2. A process according to Claim 1, wherein the catalyst is selected from the group consisting of alumina, titania, zirconia, silica, a mixture of titania and zirconia, a mixture of alumina and magnesia, a mixture of alumina and titania and a mixture of alumina and silica.
3. A process according to Claim 1, wherein the catalyst comprising a mixture of alumina and titania is in a weight ratio of alumina to titania of 75-98 : 25-2.
4. A process according to Claim 3, wherein the catalyst comprising a mixture of alumina and titania is a catalyst prepared from boehmite as an alumina raw material.
5. A process according to Claim 3, wherein the catalyst comprising a mixture of alumina and titania is a catalyst prepared from titanium sulfate as a titania raw

material.

6. A process according to Claim 3, wherein the catalyst comprising a mixture of alumina and titania is a catalyst prepared by adding sulfuric acid thereto during the catalyst preparation.

7. A process according to Claim 3, wherein the catalyst comprising a mixture of alumina and titania contains sulfate ions.

8. A process according to Claim 1, wherein the catalyst comprises a mixture of alumina, titania and at least one member selected from the group consisting of zirconia, tungsten oxide, silica, tin oxide, ceria, bismuth oxide, nickel oxide and boron oxide and having a weight ratio of at least one member selected from the group consisting of zirconia, tungsten oxide, silica, tin oxide, ceria, bismuth oxide, nickel oxide and boron oxide to sum total of alumina and titania being 0.1-10 : 99.9-90.

9. A process for treating a fluorine compound-containing gas, which comprises contacting a gas stream containing a compound comprising carbon and fluorine with a catalyst comprising a mixture of alumina, titania and zirconia, and having a weight ratio of alumina to titania being 75-98 : 25-2 and a weight ratio of zirconia to sum total of alumina and titania being 2-10 : 98-90, thereby hydrolyzing the compound comprising carbon and fluorine.

10. A process according to Claim 1, wherein the catalyst comprises a mixture of alumina and at least one

member selected from the group consisting of zinc oxide, nickel oxide, iron oxide, tin oxide, cobalt oxide, zirconia, ceria, silica and platinum and has an atomic ratio of aluminum of the alumina to at least one element of at least one of the member except for platinum being 50-99 : 50-1, and the content of platinum being 0.1 to 2% by weight per 100% by weight of the alumina.

11. A process according to Claim 10, wherein the catalyst further contains 0.1 - 20% by weight of sulfur on the basis of the catalyst.

12. A process according to Claim 12, wherein the catalyst containing sulfur comprises a mixture of alumina and nickel oxide.

13. A process for treating a fluorine compound-containing gas, which comprises contacting a gas stream containing a fluorine compound comprising  $C_2F_6$  with a catalyst comprising alumina and titania having a weight ratio of alumina to titania being 65-90 : 35-10, thereby hydrolyzing the fluorine compound to convert the fluorine in the gas stream to hydrogen fluoride.

14. A process for treating a fluorine compound-containing gas, which comprises contacting a gas stream containing a fluorine compound comprising  $C_2F_6$  with a catalyst comprising alumina, titania and zirconia and having a weight ratio of alumina to titania being 65-90 : 35-10 and a weight ratio of zirconia to sum total of alumina and titania being 2-10 : 98-90, thereby hydrolyzing the fluorine compound to convert the fluorine

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in the gas stream to hydrogen fluoride.

15. A process for treating a fluorine compound-containing gas, which comprises contacting a gas stream containing a fluorine compound comprising at least one member selected from the group consisting of  $C_2F_6$ ,  $CF_4$ ,  $C_4F_8$  and  $CHF_3$  with a catalyst comprising a mixture of alumina and zinc oxide and having an atomic ratio of aluminum to zinc being 90-70 : 10-30, thereby hydrolyzing the fluorine compound to convert the fluorine in the gas stream to hydrogen fluoride.

16. A process for treating a fluorine compound-containing gas, which comprises a gas stream containing a fluorine compound comprising at least one member selected from the group consisting of  $C_2F_6$ ,  $CF_4$ ,  $C_3F_8$ ,  $C_4F_8$ ,  $CHF_3$ ,  $NF_3$  and  $SF_6$  with a catalyst comprising a mixture of alumina and nickel oxide and having an atomic ratio of aluminum to nickel being 95-60 : 5-40, thereby hydrolyzing the fluorine compound to convert the fluorine in the gas stream to hydrogen fluoride.

17. A process for treating a fluorine compound-containing gas, which comprises contacting a gas stream containing a fluorine compound comprising  $C_4F_8$  with a catalyst comprising a mixture of alumina and nickel oxide, thereby hydrolyzing the fluorine compound to convert the fluorine in the gas stream to hydrogen fluoride.

18. A process according to Claim 16, wherein a reaction temperature is 650° - 800°C for the hydrolysis

of  $C_2F_6$ ,  $600^\circ - 800^\circ C$  for the hydrolysis of  $CF_4$  and  $CHF_3$ ,  $700^\circ - 800^\circ C$  for the hydrolysis of  $C_3F_8$ ,  $650^\circ C - 800^\circ C$  for the hydrolysis of  $C_4F_8$ ,  $600^\circ - 800^\circ C$  for the hydrolysis of  $NF_3$  and  $500^\circ - 800^\circ C$  for the hydrolysis of  $SF_6$ .

19. A process according to Claim 15, wherein a reaction temperature is  $650^\circ - 800^\circ C$  for the hydrolysis of  $C_4F_8$  and  $600^\circ - 800^\circ C$  for the hydrolysis of  $CF_4$  and  $CHF_3$ .

20. A process for treating a fluorine compound-containing gas, which comprises a hydrolysis step of contacting a gas discharged from a semiconductor-etching or cleaning step using a gas stream containing at least one fluorine compound selected from the group consisting of compounds of carbon and fluorine, compounds of carbon, hydrogen and fluorine, compounds of sulfur and fluorine, compounds of nitrogen and fluorine and compounds of carbon, hydrogen, oxygen and fluorine, after addition of air and steam to the gas, with a catalyst comprising at least one of alumina, titania, zirconia and silica, thereby hydrolyzing the fluorine compound to convert the fluorine in the gas to hydrogen fluoride, as a poststep to the semiconductor-etching or cleaning step.

21. A process according to Claim 20, which further comprises an alkaline washing step of contacting the gas from the hydrolysis step with an alkaline washing solution, thereby washing the gas as a poststep to the hydrolysis step.

ABSTRACT OF THE DISCLOSURE

A gas stream containing at least one fluorine compound selected from the group consisting of compounds of carbon and fluorine, compounds of carbon, hydrogen and fluorine, compounds of sulfur and fluorine, compounds of nitrogen and fluorine and compounds of carbon, hydrogen, oxygen and fluorine is contacted with a catalyst comprising at least one of alumina, titania, zirconia and silica, preferably a catalyst comprising alumina and at least one of nickel oxide, zinc oxide and titania in the presence of steam, thereby hydrolyzing the fluorine compound at a relatively low temperature, e.g. 200° - 800°C, to convert the fluorine of the fluorine compound to hydrogen fluoride.

FIG. 1

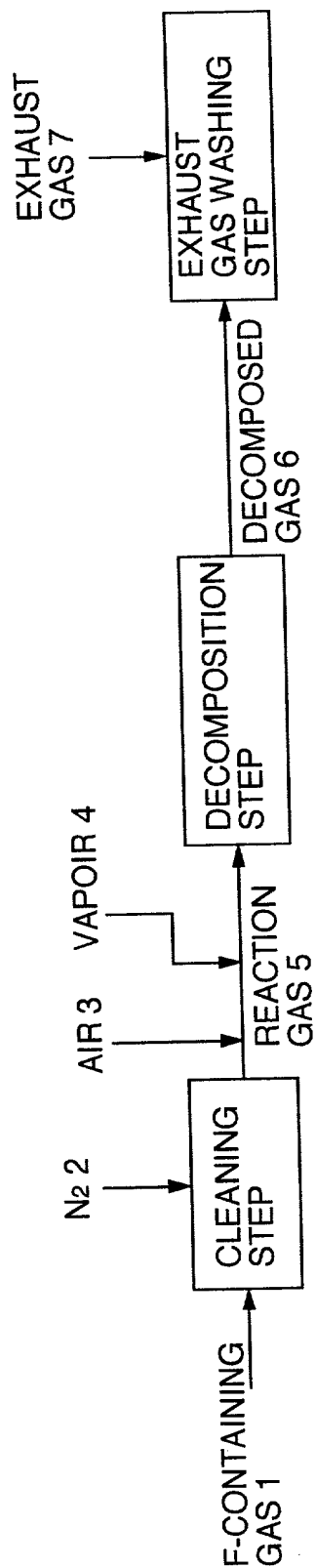


FIG. 2

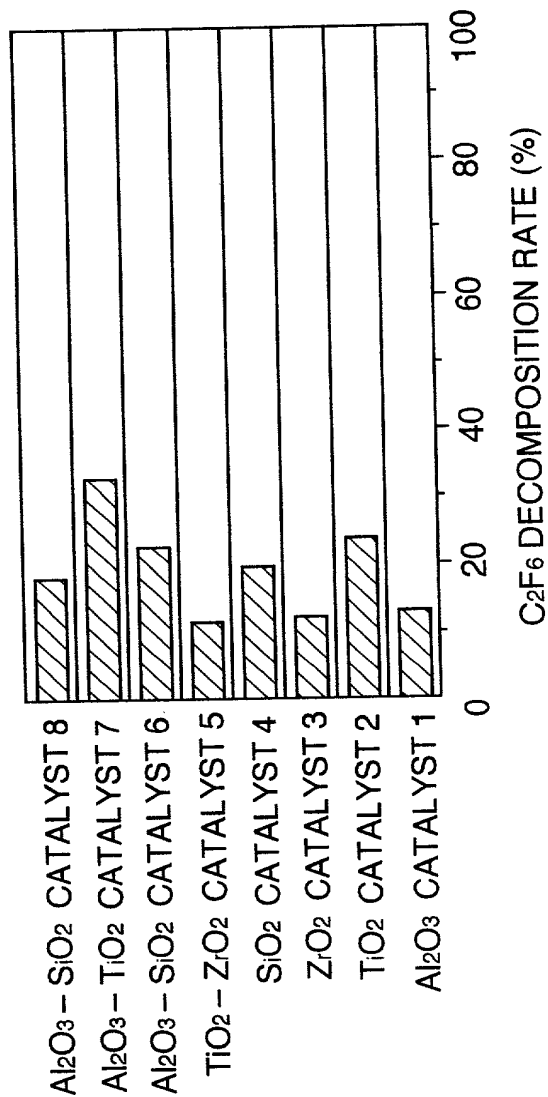




FIG. 3

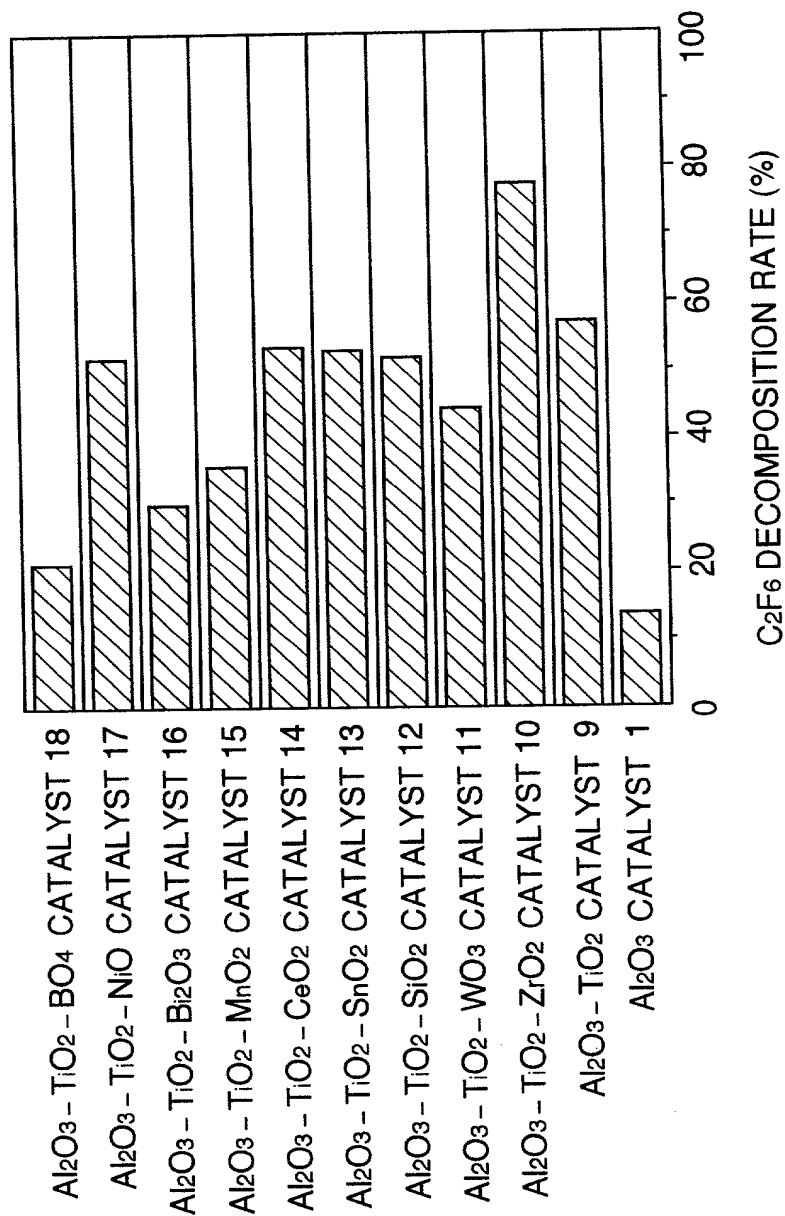


FIG. 4

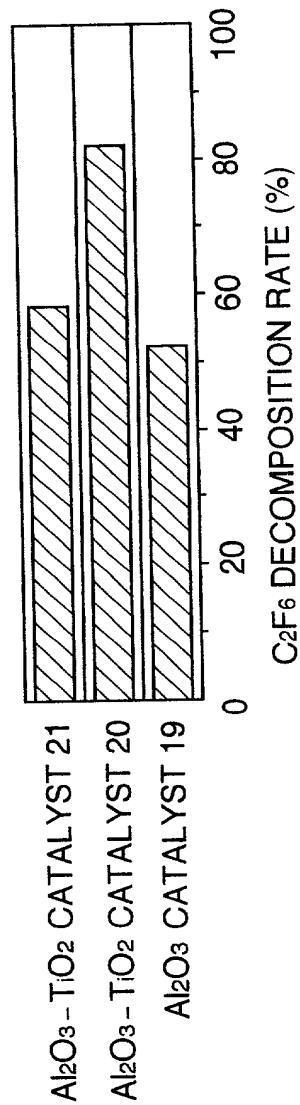


FIG. 5

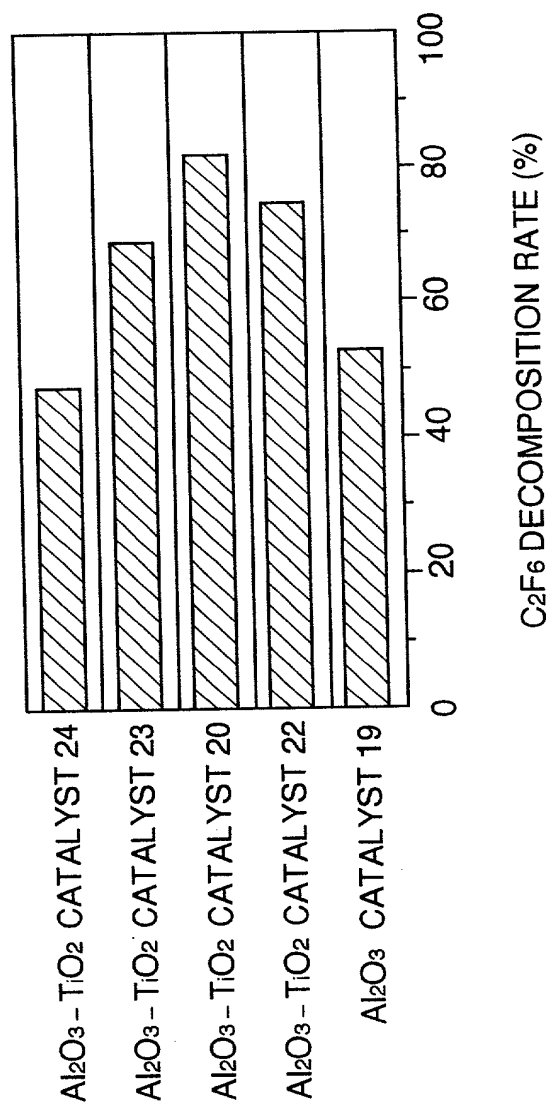


FIG. 6

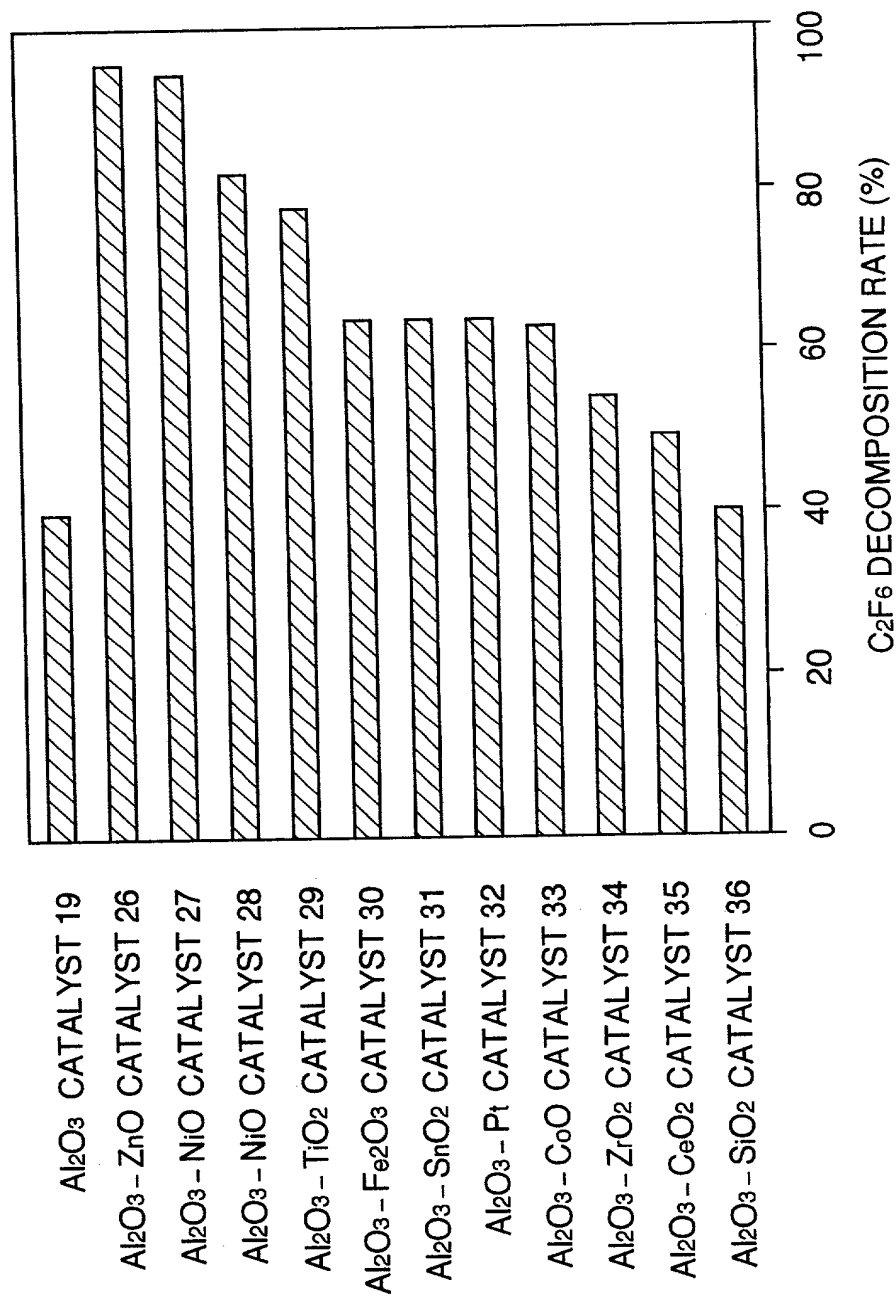


FIG. 7

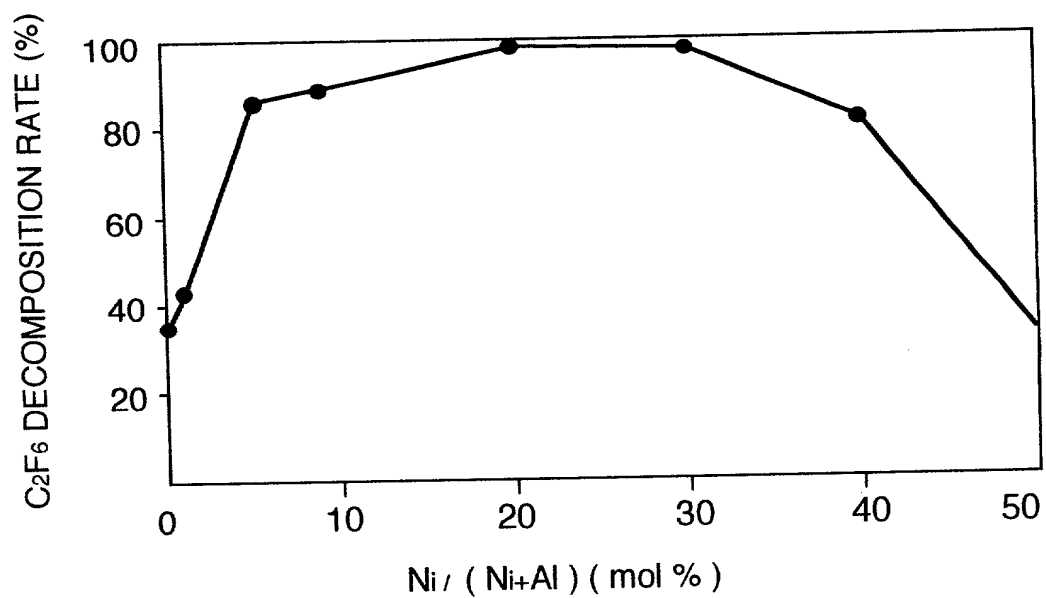


FIG. 8

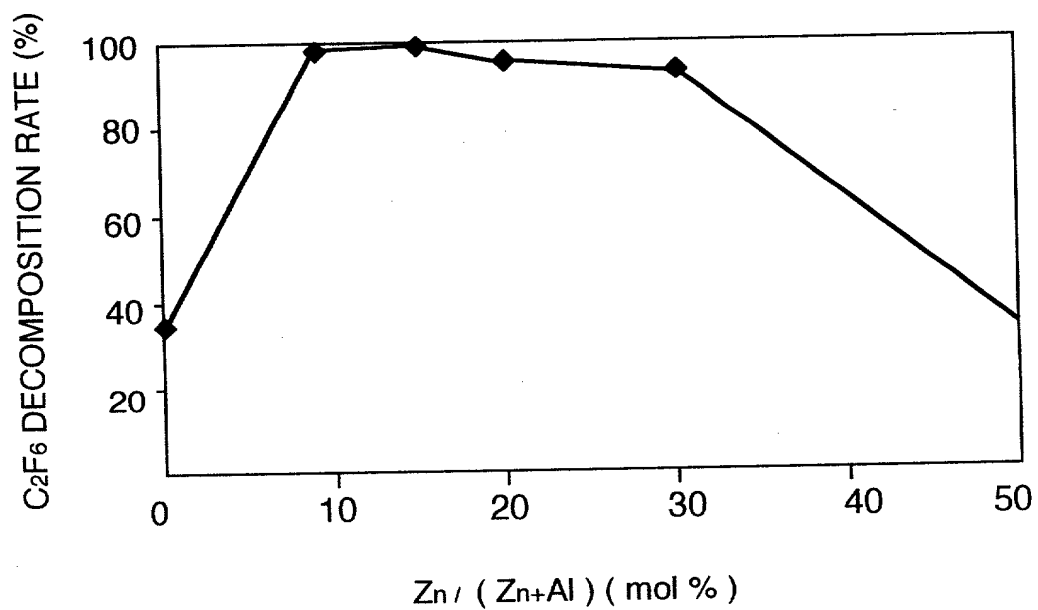


FIG. 9

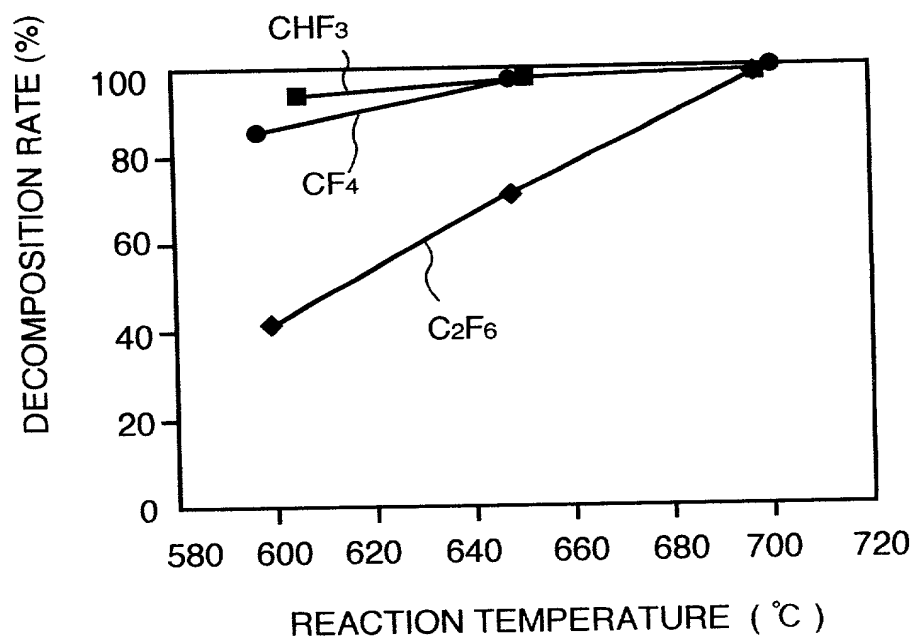


FIG. 10

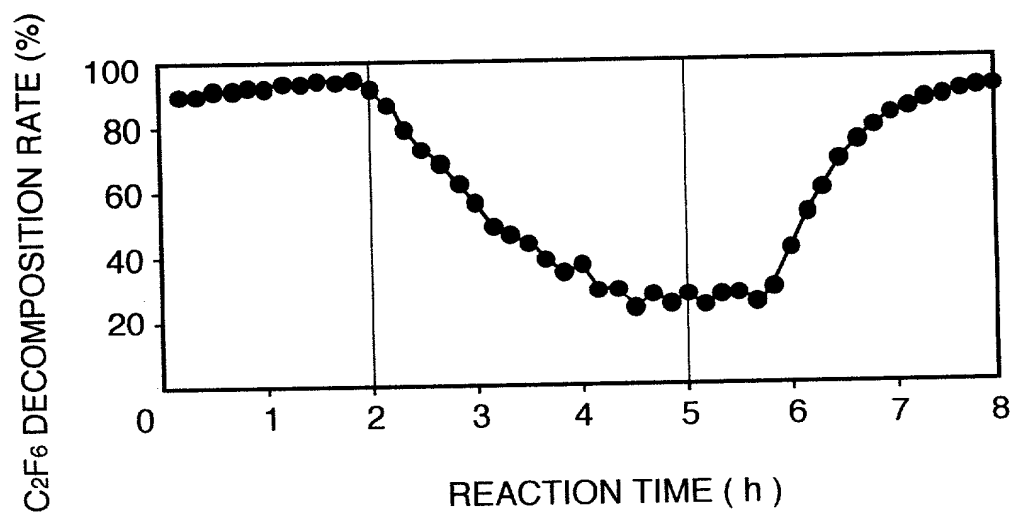


FIG. 11

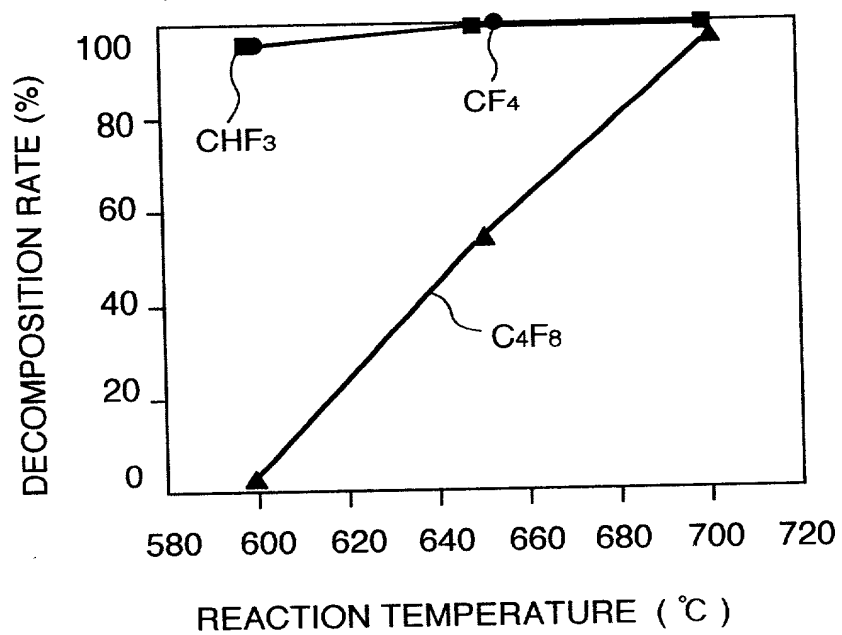


FIG. 12

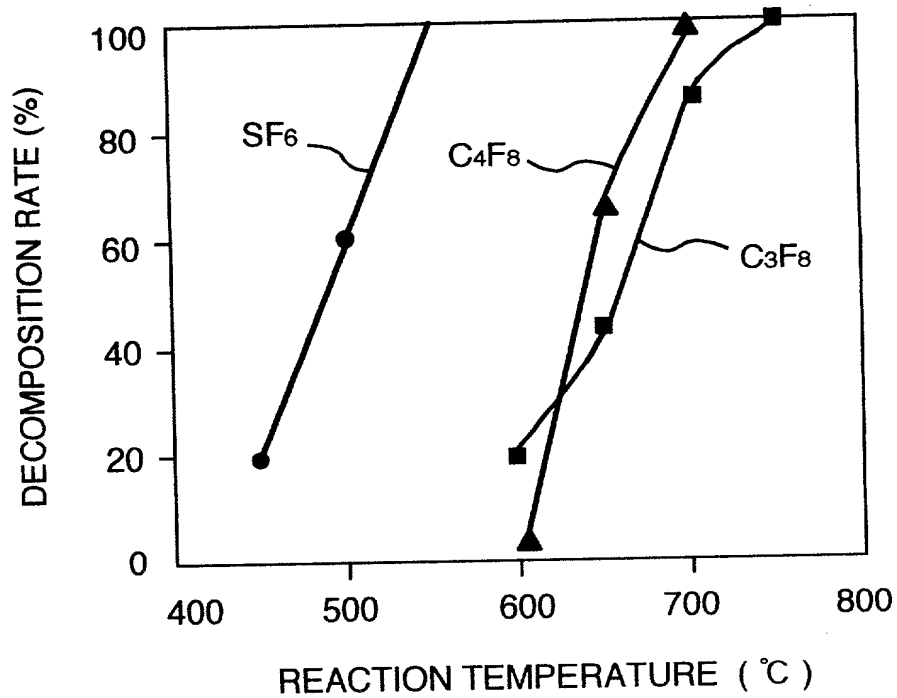
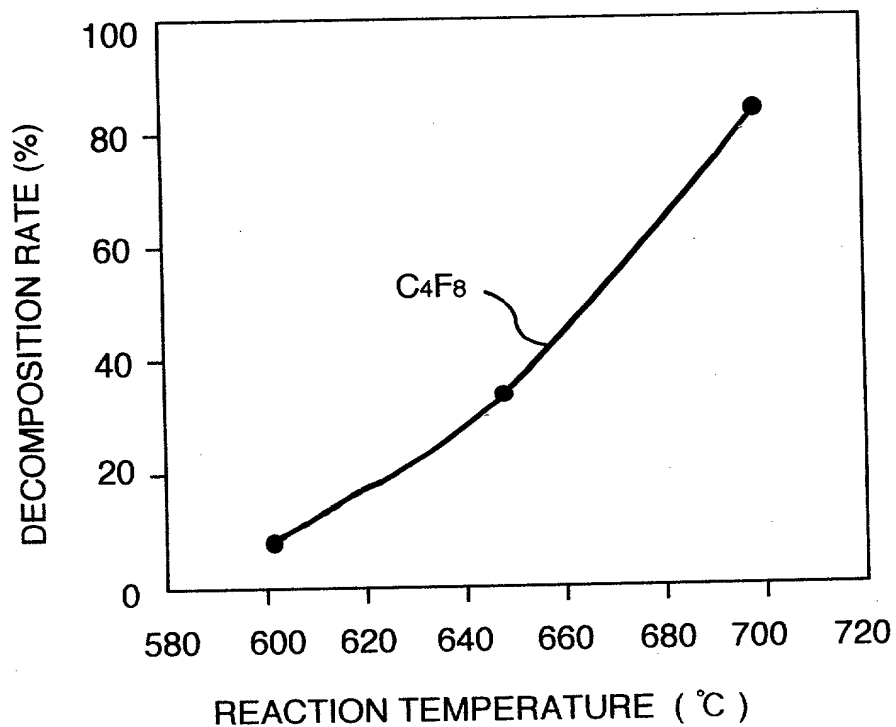
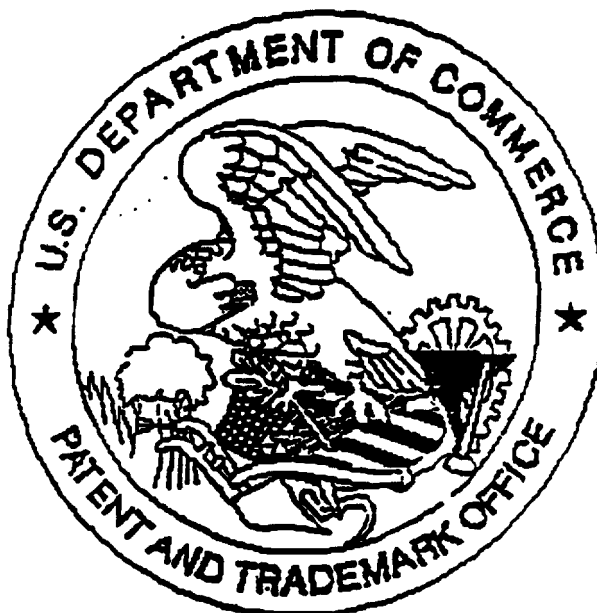


FIG. 13



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